

AMENDMENTS

In the Claims:

Please cancel claims 1-16 without prejudice or disclaimer and add new claims 17 to 27 as follows:

-- 17. A process for preparing an enhanced plant nutrient value composition from a low analysis waste material, comprising:

pumping a slurry form of the low analysis waste material through a pipe reactor for reaction with at least one base or acid to form a high temperature melt;

spraying the melt from the pipe reactor directly onto a recycling bed of fines in a granulator, and flashing off water contained in the melt as steam;

rolling the melt onto particles in the granulator to form granulated particles; and

drying the granulated particles to reduce the moisture content thereof to form dried granulated particles comprising an enhanced plant nutrient value composition.

18. A process as recited in claim 17, wherein the pipe reactor is located within the granulator.

19. A process as recited in claim 18, wherein the granulator is a rotating cylinder.

20. A process as described in claim 17, wherein the pipe reactor comprises two cross pipes.

21. A process as described in claim 20, wherein two acids are introduced via the two cross pipes.

22. A process as described in claim 21, wherein the two acids are sulphuric acid and phosphoric acid.

23. A process as described in claim 17, wherein the temperature is maintained to less than 149 degrees centigrade.
24. A process as described in claim 17, further comprising the addition of water to the low analysis waste material to form a slurry prior to pumping.
25. A process as described in claim 17, wherein the high temperature melt is produced by a pipe reactor that is located within the granulator.
26. A process as described in claim 25, wherein the pipe reactor for producing the high temperature melt has a length for mixing the slurry with material from at least one cross pipe of at least 51 centimeters.
27. A process as described in claim 17, wherein the melt is produced in a pipe reactor having a diameter of approximately 7.6 centimeters to 25.4 centimeters, a length of approximately 2.1 meters to 15.4 meters and terminates in a 5 centimeter to 20 centimeter discharge pipe or slot of equivalent cross-sectional area into the granulator. --

REMARKS

Claims 1-16 are pending. Claims 1-13 have been rejected on 102, 103, and double patenting grounds. Claims 14 to 16 have been rejected on double patenting grounds.

In response, all claims have been cancelled. Old claims 14 to 16 have been re-written with additional claim elements as new claims 17 to 27. The added language in the new claims recite the feature of direct transfer of melt from the reaction pipe into the granulator, which is described throughout the specification, for example at the bottom of page 6, the seventh line of page 7, and in Figure 3. The dimensions recited in claims 26 and 27 are, for example, provided at the bottom of page 6 through the first paragraph of page 7. . The temperature recited in claim